

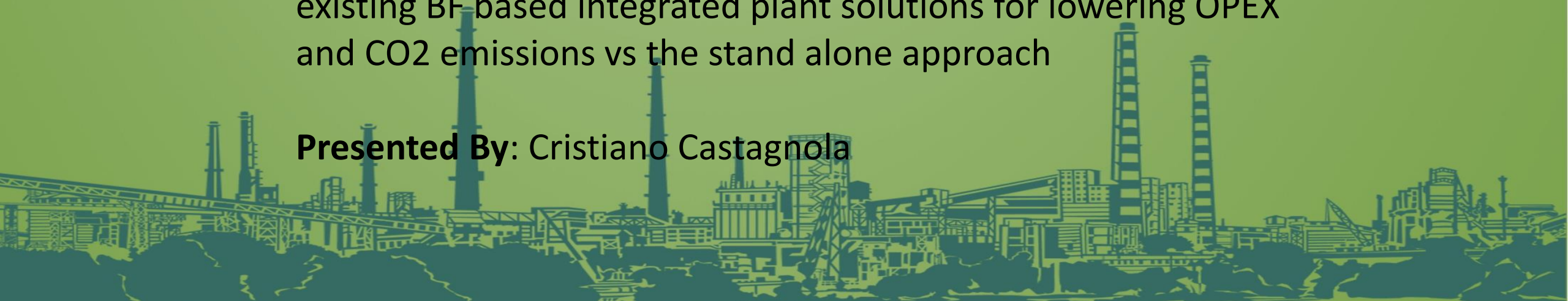
Presents

International Conference on
GREEN & SUSTAINABLE IRON MAKING

January 17 – 18, 2024

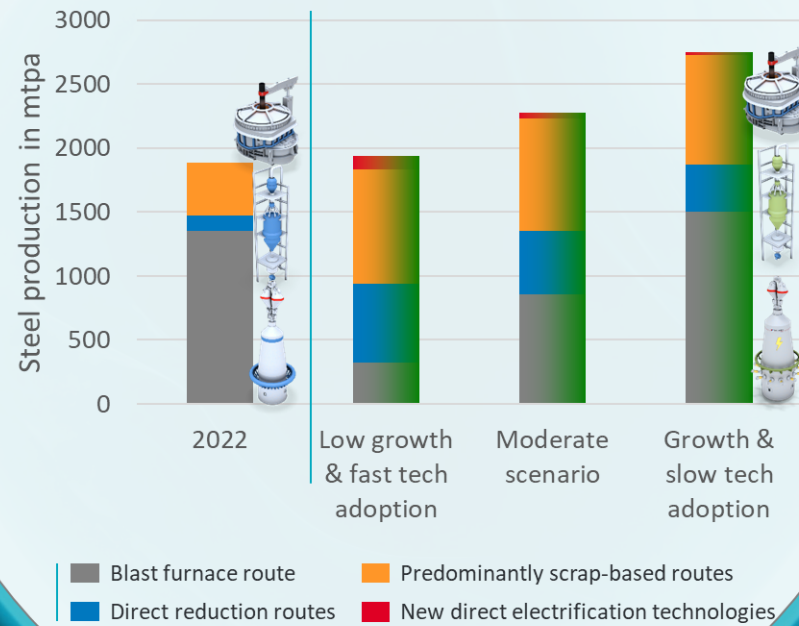
Title of Paper: Smart combination of new Midrex DR plants in existing BF based integrated plant solutions for lowering OPEX and CO₂ emissions vs the stand alone approach

Presented By: Cristiano Castagnola



2050

Global Steel Demand & Production Technology Mix



Decarbonisation pathways for ore based steel making

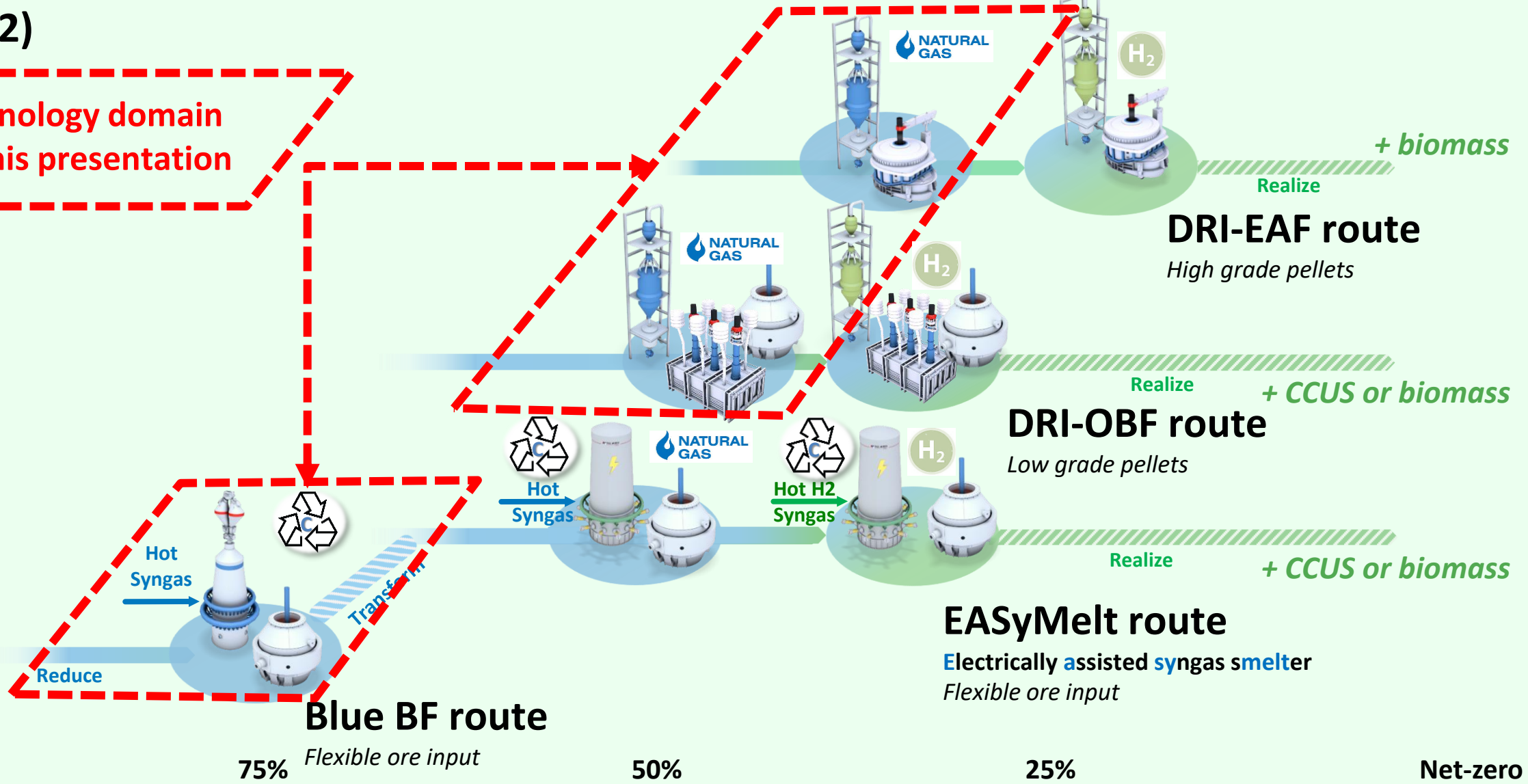
(Scope 1+2)

Technology domain of this presentation



Today

100%



SCOPE 1+2 EMISSIONS Scope 2 calculated with Ele. Power emission factor of 80kg CO₂/MWh (target 2050)

Main challenges for BF based decarbonization of integrated steel plants

Availability of Iron ore pellets with different specification vs BF use

Limited flexibility of BF route vs variable market conditions

Iron ore pellets waste material management once sinter plants are outpaced

Availability of green hydrogen in required quantity & consistent with the continuous needs of industrial plant

Unpredictable evolution of natural gas, coal and electrical energy costs

Increased dependency of the steel production cost to electrical power availability and cost

Evolution of CO2 taxation scheme decoupled with steel market development

Metallurgy of high end steel qualities requiring low nitrogen levels in steels

Challenges addressed by this presentation

NG Midrex Direct reduction Technology (NG DRP)

MIDREX

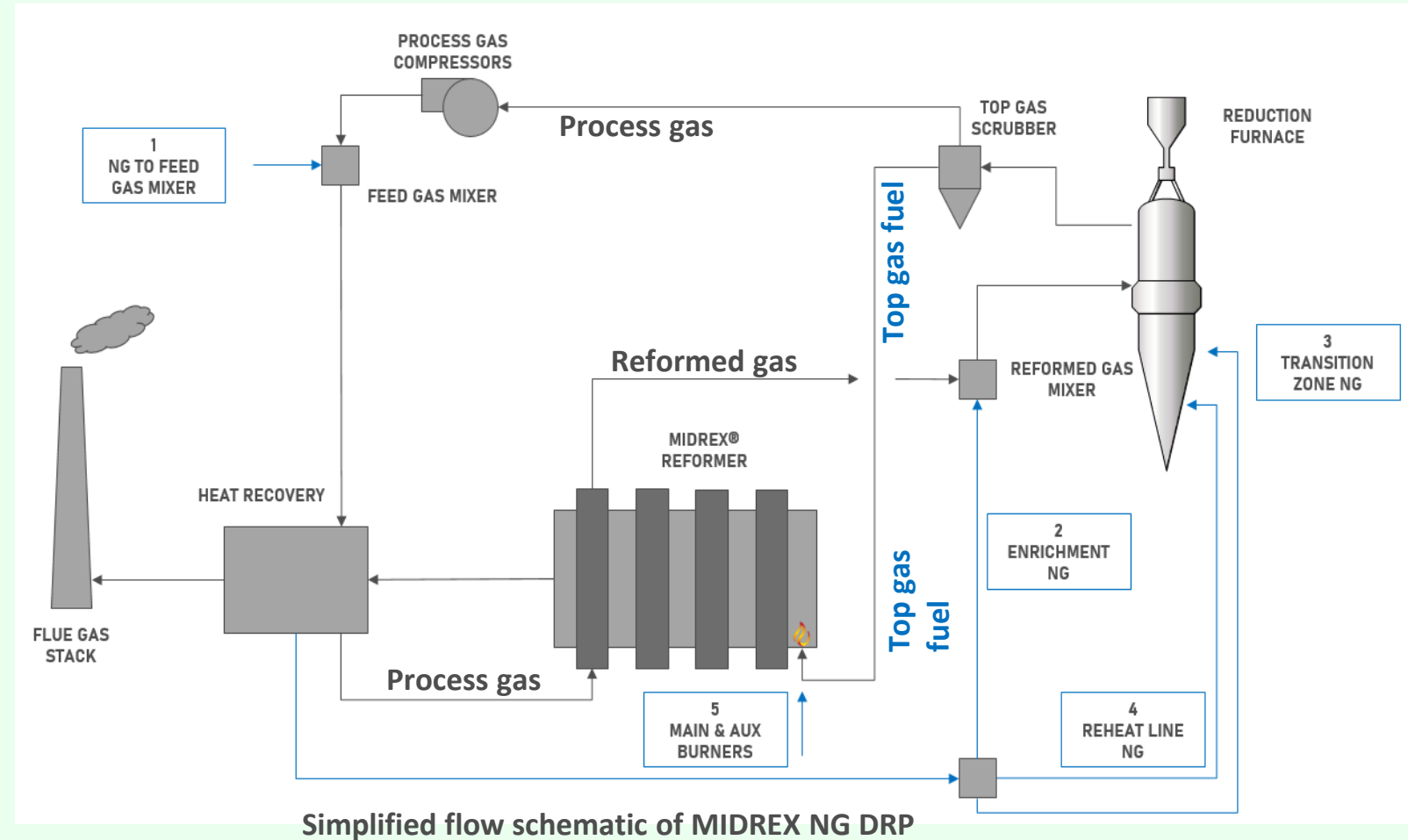
Focus on gas looping

NG Process use

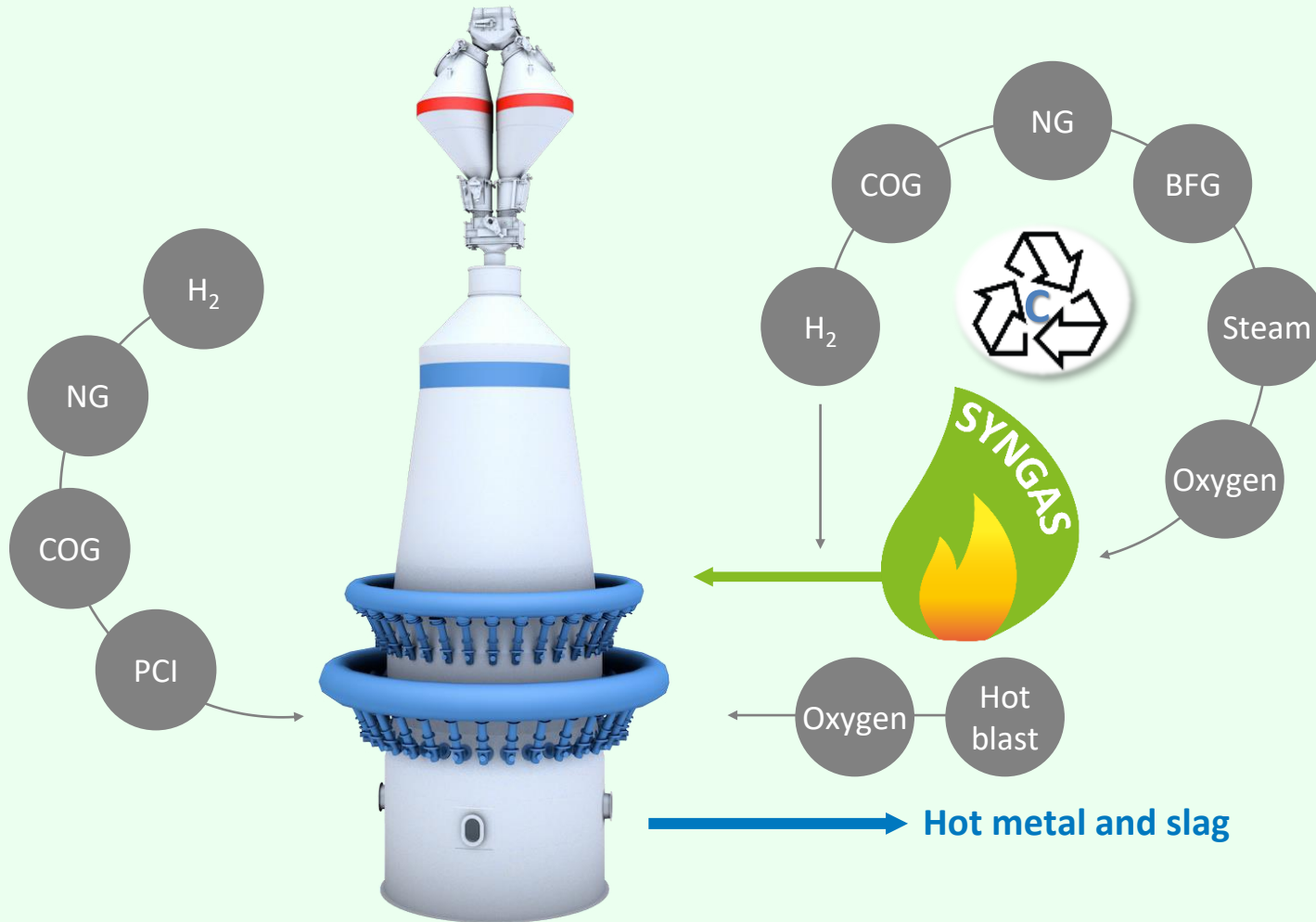
1. Feed gas mixer (NG make up)
2. Enrichment at reformed gas
3. Transition zone
4. Reheat line

NG Thermal use

5. Feed to burners of Reformer mixed with top gas fuel



Blast Furnace (Blue BF) modified to use Syngas for reducing OPEX & CO₂ footprint



Hot syngas shaft injection

- › Enabler for higher top gas temperature
- › Allows higher amounts of auxiliary fuel injection at tuyère level (e.g. COG, NG, H₂, syngas)

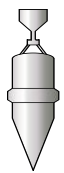
Main effect of hot syngas injected at BF shaft

- › CO₂ emission reduction up to 28 % (only syngas)
- › Reduced OPEX due to coke rate decrease
- › Productivity increase due to decreased gas generation at bosh level

The way to smartly integrate a Midrex DRP into traditional BF BOF steelmaking

how to maximize metallurgical gases valorisation

STEP 0



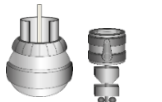
Direct Reduction Plant (DRP)
as island

BF BOF steel making as island

COKE OVEN PLANT



BLAST FURNACE

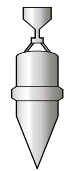


BOF/CONPRO & CASTER



POWER PLANT

STEP A



DRP is a receiver

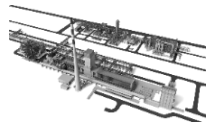


NG Input

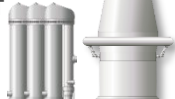


Gas delivery

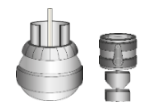
BF BOF



COKE OVEN PLANT



BLAST FURNACE



BOF/CONPRO & CASTER



POWER PLANT

STEP B



Blue DRP fully integrated



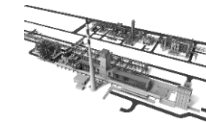
NG Input



Gas exchange

PATENT PENDING

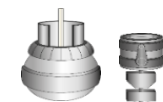
BLUE BF BOF



COKE OVEN PLANT



BLUE BLAST FURNACE

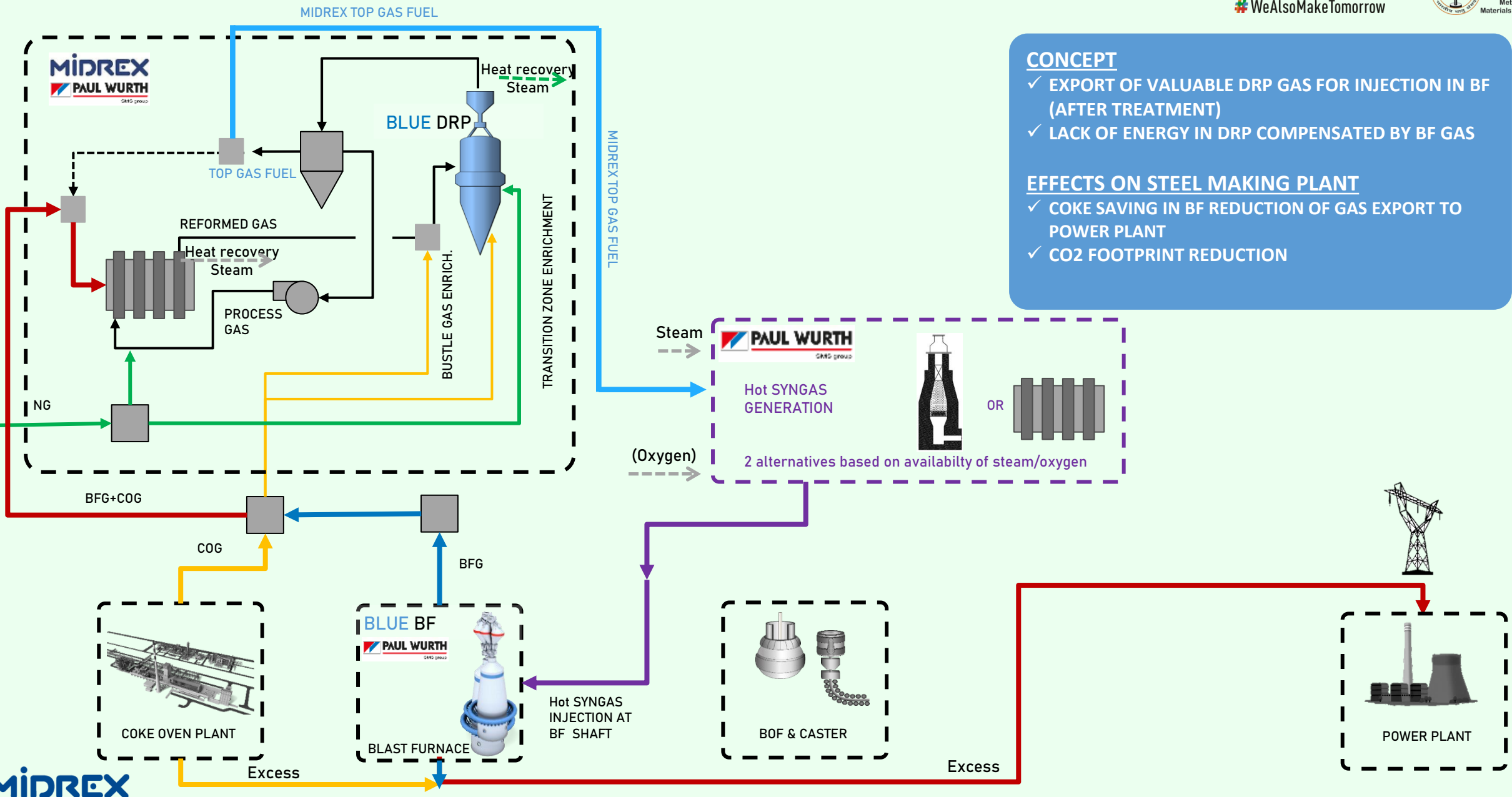


BOF/CONPRO & CASTER



POWER PLANT

BLUE BF in smart combination with DRP through gas exchange



CONCEPT

- ✓ EXPORT OF VALUABLE DRP GAS FOR INJECTION IN BF (AFTER TREATMENT)
- ✓ LACK OF ENERGY IN DRP COMPENSATED BY BF GAS

EFFECTS ON STEEL MAKING PLANT

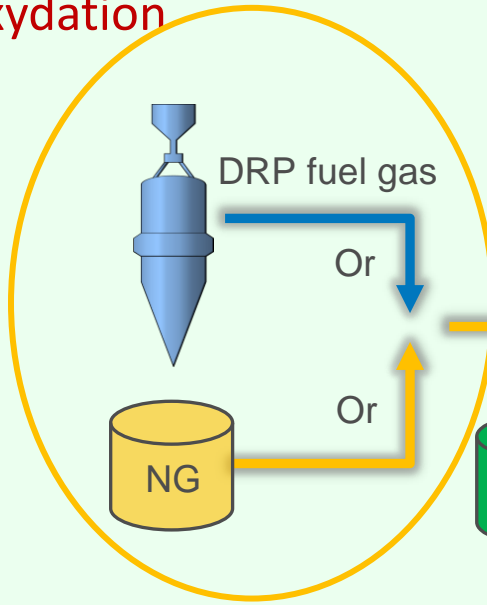
- ✓ COKE SAVING IN BF REDUCTION OF GAS EXPORT TO POWER PLANT
- ✓ CO2 FOOTPRINT REDUCTION

BLUE BF in smart combination with DRP through gas exchange

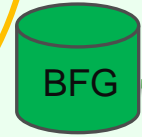
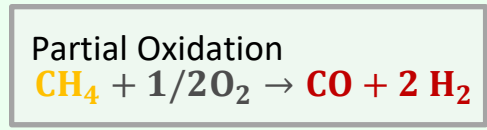
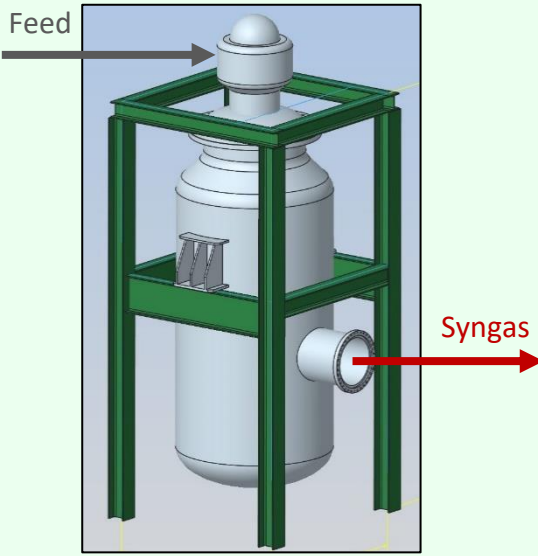
Syngas generation applied to Midrex fuel gas to generate hot syngas

Alternative 1: Catalytic Partial Oxidation

- Syngas is produced by partial combustion of natural gas or DRP Fuel gas
- Possible to use C2+ rich feedstocks
- High syngas quality



APPLIED when OXYGEN is available

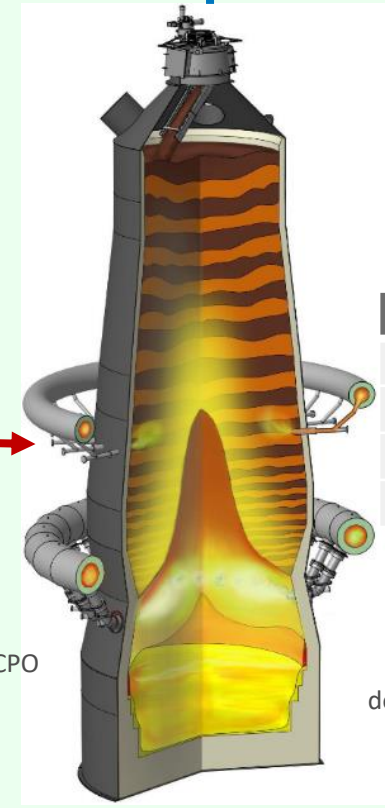


Syngas
900°C

Syngas composition	
CH ₄	<1 vol.-%
CO	28 vol.-%
CO ₂	2 vol.-%
H ₂	58 vol.-%
H ₂ O	7 vol.-%
N ₂	3 vol.-%

Figures for NG fed CPO

PATENT PENDING



BF gas typical composition		
CO	20-23	vol.-%
CO ₂	20-23	vol.-%
H ₂	9-12	vol.-%
N ₂	balance	vol.-%

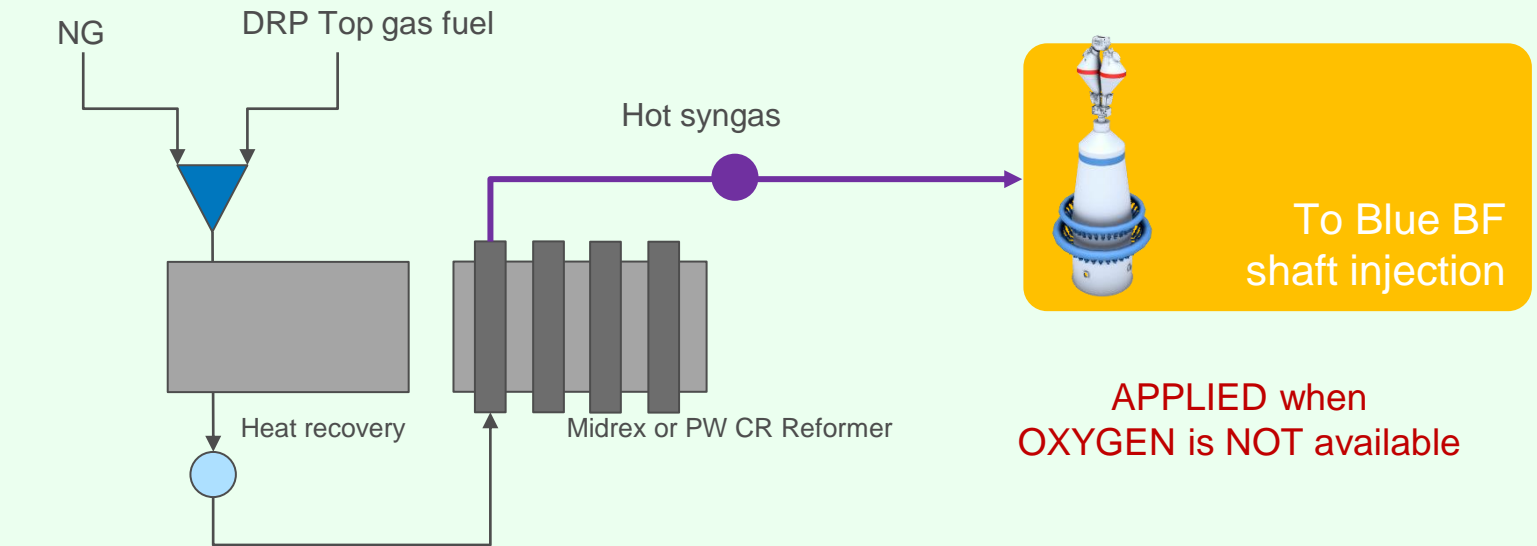
BF gas with syngas injection has significant changes → higher L.H.V. and re-use in downstream facilities (incl. fuel to Midrex Reformer)

BLUE BF in smart combination with DRP through gas exchange

Syngas generation applied to Midrex Top gas fuel to generate hot syngas
Alternative 2: Midrex or PW Combined Reforming additional reformer



Hot Syngas generation through Catalytic reforming of Midrex Top gas fuel



	H ₂ [mol %]	CO [mol %]	CO ₂ [mol %]	H ₂ O [mol %]	CH ₄ [mol %]	N ₂ [mol %]	TEMP
INLET	35	19	15	13	17	1	580°C
OUTLET	55	35	2	6	1	1	950 °C

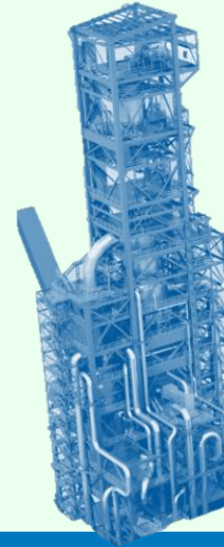


BLUE BF in smart combination with DRP through gas exchange: OPEX and CO2 (*)



ASSUMED UTILITIES AND RAW MATERIAL COSTS

Parameter	uom	Cost
DR grade pellets	€/t	176
BF grade pellets	€/t	144
Sinter feed	€/t	72
Coking coal (variable)	€/t	410
CO ₂	€/t	0
Electrical power (variable)	€/kWh	0,098
Natural Gas (variable)	€/GJ	30,2
Scrap	€/t	456
Sludge disposal	€/t	0
Manpower	€/h	10

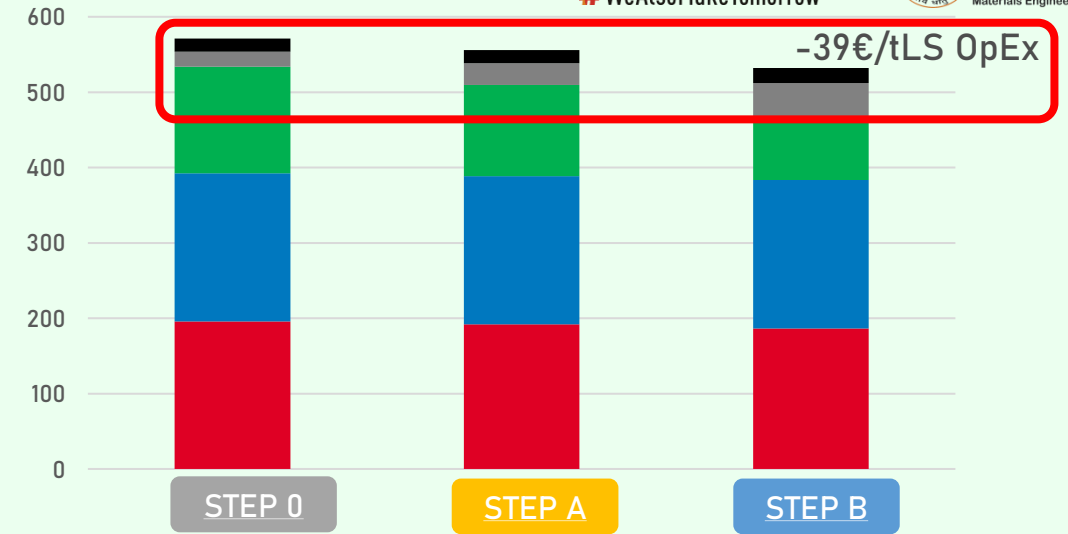
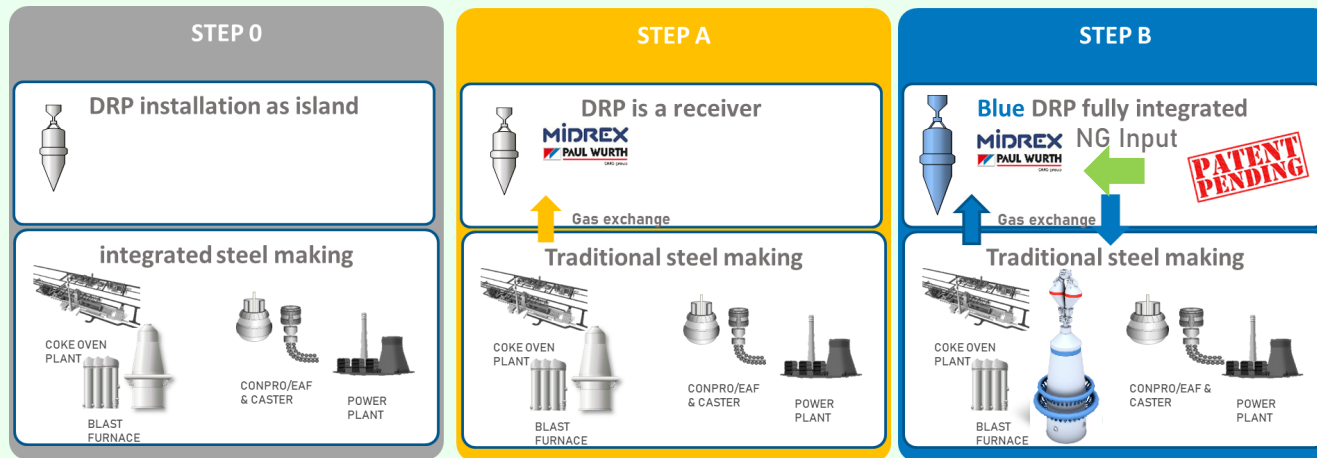


Blue BF's

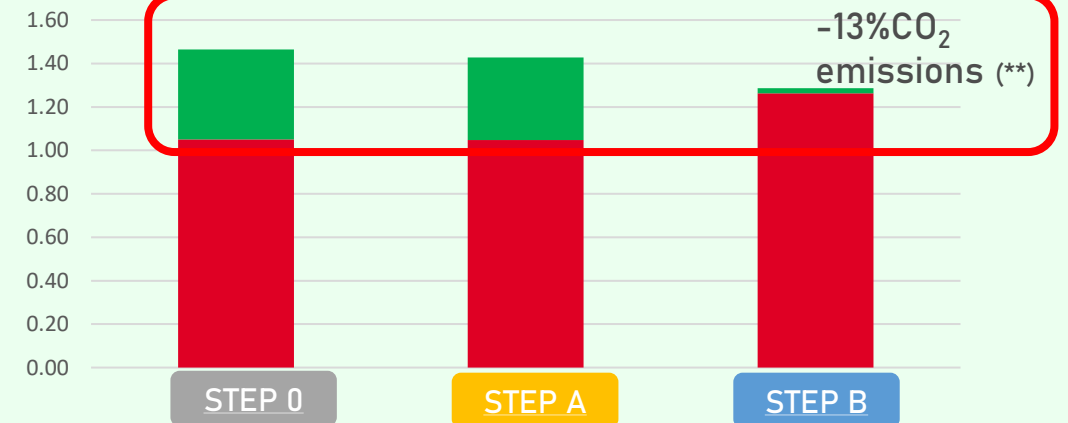
4 MTPY HM production

1 DRP

2,5 MTPY DRI production



■ Work & Maintenance
■ Grid electrical power
■ Chemical energy (NG, H2)
■ Processed Raw material (pellets, ore, scrap)
■ Primary raw material (coal, sinter feed)



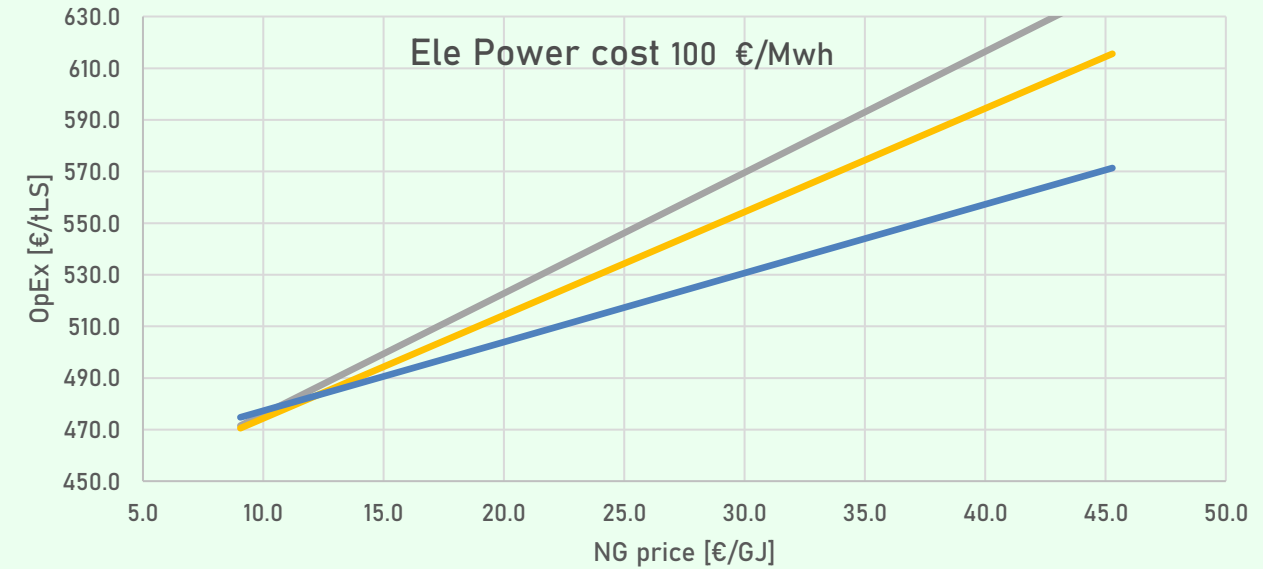
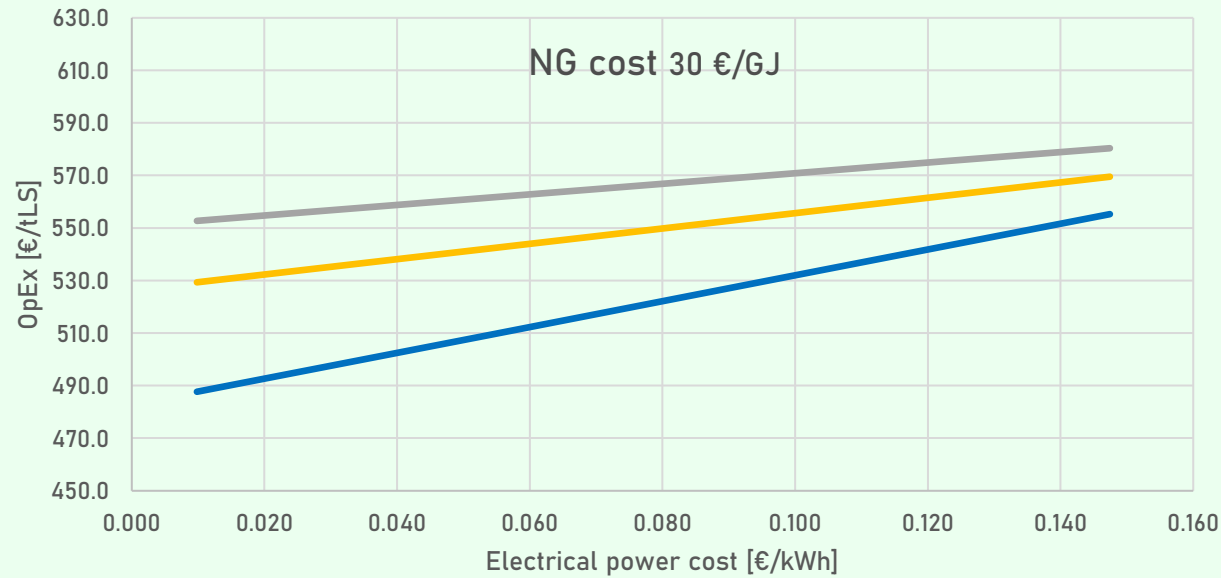
■ CO2 Emission scope 1 - Direct t/t LS
■ CO2 Emission scope 1 - indirect t/t LS

(*) Considering CPO for syngas generation

(**) on approx. 7 MTPY LS produced through BF or DRP routes as islands

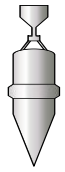
BLUE BF in smart combination with DRP through gas exchange: OPEX sensitivity

UTILITIES AND RAW MATERIAL COSTS AS PER PREVIOUS SLIDE



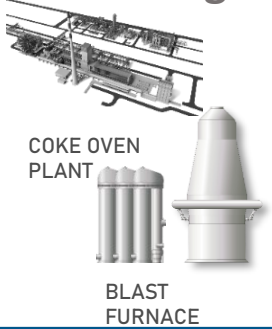
BLUE BF in smart combination with DRP through gas exchange: flexibility vs energy cost

STEP 0

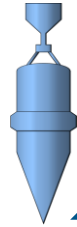


DRP installation as island

integrated steel making



STEP B



Blue DRP fully integrated



NG Input

PATENT PENDING

Gas exchange

Traditional steel making



STEP C

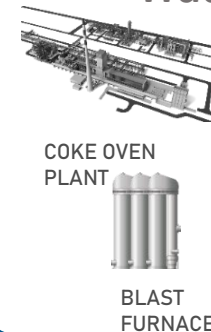


DRP installation as island



NG Input

Traditional steel making



NG Input



Blue BF with CPO syngas production can be fed either with DRP fuel gas (STEP B) or NG (STEP C)

Blue BF with CPO can be integrated with Blue DRP or operated Stand-alone based on market conditions

Higher cost ratio of NG/coal

Lower cost ratio of NG/coal

Main takeaways

The use of NG as a needed transition reductant in place of green hydrogen can be optimized when a Midrex DRP is installed in an existing BF based integrated plant

The proposed solution of bi-directional gas exchange between Blue BF and Midrex DRP is beneficial in terms of OPEX and CO₂ emissions

The needed technologies to smartly integrate an NG based Midrex DRP in a BF based steel plant are proven and readily available

The proposed solution is best placed to ensure the OPEX competitiveness in case the relative costs of reducing agents (NG , coal and H₂) change

SMS  group

MIDREX

The information provided in this presentation contains a general description of the products concerned. The actual products may not always have these characteristics as described and, in particular, these may change as a result of further development of the product. The provision of this information is not intended to have and will not have legal effect.

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